## Magnetic nanoparticles incorporated in CALF-20 MOF for MISA assisted separation of $CO_2/N_2$ in post combustion mixtures

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Calgary Framework CALF-20 demonstrated to preferentially adsorb CO<sub>2</sub> over H<sub>2</sub>O in post-combustion mixtures. Main advantages INDUCTION HEATING CAN TRIGGER THE REGENERATION OF SORBENT BEDS: Classically, the heat in a Temperature Swing Heat is generated directly inside the sorbent bed; no heat Adsorption (TSA) process is supplied indirectly by using a pre-Lin et al. Science 374,1464,2021 heated purge gas. Such method implies energy wastes at the outlet and the need to upgrade or purify the output stream from transfer resistance the purge dilution. By implementing MAGNETIC COMPOSITES ADSORBENTS such as magnetic nanoparticles embedded in MOF, Very quick start up of desorption (ΔT>100°C/min) allows increased productivity heat can be generated in-situ by applying an alternating magnetic field. This is a fully electrified regeneration process named lelps decarbonizing Magnetic Induction Swing Adsorption (MISA). chemical industry using sustainable electricity Synthesis and shaping of  $Fe_3O_4$  @ CALF-20 composite Sustainable synthesis by Fe<sub>3</sub>O<sub>4</sub> @ CALF-20 The Liquid Assisted Grinding: 1 Triazole 1.25g Zinc Oxalate =1.65g composite was shaped into granules using a 5% (w/w) hour milling Mixer/Mill. Ball Spex in to powder Methanol = 2ml weight ratio 10. Washing in Poloxamer acqueos solution. The solution was water sprayed onto the powder The Fe<sub>3</sub>O<sub>4</sub> nanoparticles were synthesized in a specifically ped jar and kept by thermal placed decomposition of developed jar iron Magnetic MOF rotating (80Hz for 8 hours) using a roll jar mill. acetylacetonate in high boiling Fe<sub>3</sub>O<sub>4</sub> nanoparticles solvent, in the presence of Powder (0.29g) Granules surfactants Characterization of Fe<sub>3</sub>O<sub>4</sub> @ CALF-20 composite CALF20\_1H COMPOSITE 300 275 Fe<sub>3</sub>O<sub>4</sub> - Fe<sub>2</sub>O CALF20 adsorption CALF20-Fe<sub>3</sub>O<sub>4</sub> 250 (a.u.) CALF20 desorption 60 225 Fe3O4@CALF20 adsorptio (cm<sup>3</sup>/d) 175 Magnetization (Am<sup>2</sup>/kg<sub>Fe</sub> 40 Fe3O4@CALF20 des ntensity 20 150 -Volume ( 0 125 -20 100 -40 75 -60 50 -20 30 40 50 60 10 70 80 90 25 -80 2theta (degree) -100 0.2 0.4 0.6 0.0 XRD Analysis performed on powders degassed at 180°C and closed in glass Applied field (T) P/P<sub>0</sub> capillary show the typical diffractogram of CALF-20 with additional peaks belonging to Fe<sub>3</sub>O<sub>4</sub>. The **TEM** images show that the magnetic nanoparticles are well dispersed on the Magnetic properties of the composites and Nitrogen adsorption/desorption isotherms at 77K Nitrogen adsorption/desorption isotherms at 77/K exhibits a type-1 + type II (IUPAC) shape, typical of microporous materials followed by non horizontal plateau with negligible mesoporosity. The more pronounced inclination of the adsorption curve at intermediate pressure regimes measured for the composite is attributable to the presence of nanoparticles that contribute a proprincence of the composite stat bare magnetite nanoparticles surface of the MOF. contribute to a non microporous surface. CO<sub>2</sub> adsorption/desorption The specific surfaces of CALF20 and Fe<sub>3</sub>O<sub>4</sub>@CALF20 calculated by BET method are  $320\pm16$  m<sup>2</sup>/g <sup>-1</sup> and CO2 273k 280±16 m<sup>2</sup>/g respectively CO2 298K CO2 308K CO2 318K CO2 328K CO2 403K 3,0 ¢ 1.4 80 Adsorption Desorption (<sup>2,5</sup> (<sup>6</sup>/loum) 60 1.2 <sup>140</sup> ູູົ N2 273K N2 298K 1.0 N2 308K ട്ല 1,5 Adsorbed 0,5 <mark>문</mark> 30 CONCLUSIONS ₹ 25  $Fe_3O_4@CALF-20$  magnetic composite has been produced by mechanochemical synthesis in 1 hour. The obtained material heats up under the effect of 0.4 පී 20 60 15 0.2 0.0 an alternating magnetic field allowing a fast desorption of the adsorbed carbon dioxide. 0.0 Ó 20 40 60 80 100 100 200 300 400 500 600 700 800 0.0 0.2 0.4 0.6 0.8 1.0 1.2 1.4 1.6 Ó Pressure (kPa) Time(s) CO<sub>2</sub> desorption by induction heating CO2 adsorption isotherms have been fitted by a dual-site Langmuir model Ip= 105A, B=16.5mT, P=200W,  $Fe_3O_4@$  CALF-20 = 0.6g.  $CO_2$  20sccm N<sub>2</sub> 110sccm  $\begin{array}{c} \text{CO}_2/\text{ N}_2 \text{ Selectivity (308K)} = 37\\ \text{Working Capacity (308K-403K)} = 0.35\text{mmol/g}\\ \Delta\text{H}_{\text{CO2}}\text{=-30} \pm 4 \text{ kJ/mol} \end{array}$ 



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